

1    **Claims**

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3    1. An apparatus comprising a first chamber and a  
4       second chamber and a membrane which divides  
5       the first and second chambers; the membrane  
6       comprising a support and a catalyst;  
7       the membrane being adapted to allow passage of  
8       a first reactant from the first chamber to the  
9       second chamber through said membrane;  
10      wherein the first reactant is imparted with  
11      enough energy by the catalyst upon said  
12      passage so as to react with the second  
13      reactant.

14

15     2. Apparatus as claimed in claim 1, wherein the  
16      support is adapted to operate at temperatures  
17      exceeding 250°C.

18

19     3. Apparatus as claimed in claim 2, wherein the  
20      support comprises an inorganic support.

21

22     4. Apparatus as claimed in any preceding claim,  
23      wherein the support comprises pores and there  
24      is a graduation in the average pore radii  
25      towards one surface of the support.

26

27     5. Apparatus as claimed in any preceding claim,  
28      wherein the membrane is adapted to activate  
29      molecules of the first reactant without  
30      forming an ionic species before the reaction  
31      with the second reactant.

32

- 1    6.    Apparatus as claimed in any preceding claim,  
2        wherein the support comprises a layer with a  
3        roughened surface which has an increased  
4        tortuosity compared to the tortuosity of the  
5        rest of the support.  
6
- 7    7.    Apparatus as claimed in claim 6, wherein the  
8        relatively roughened surface is provided on an  
9        outer surface of the support.  
10
- 11
- 12    8.    Apparatus as claimed in any preceding claim,  
13        wherein a flux control layer is provided on  
14        the support.  
15
- 16    9.    An apparatus as claimed in any one of claims 6  
17        or 7, wherein a flux control layer is provided  
18        on a first surface of the support and the  
19        layer with a roughened surface is provided on  
20        an opposite surface of the support.  
21
- 22    10.   Apparatus as claimed in claim 8 or 9, wherein  
23        the flux control layer comprises an inorganic  
24        porous layer which is adapted to hold a  
25        portion of the catalyst therein and to control  
26        the passage of the first reactant through the  
27        membrane.  
28
- 29    11.   Apparatus as claimed in any one of claims 8 to  
30        10, wherein the flux control layer is selected  
31        from the group consisting of silica and gamma  
32        alumina.

- 1    12.    Apparatus as claimed in any preceding claim,  
2        wherein the catalyst comprises a metal  
3        catalyst.  
4
- 5    13.    Apparatus as claimed in claim 12, wherein the  
6        metal catalyst is selected from the group  
7        consisting of rhodium, ruthenium and nickel.  
8
- 9    14.    Apparatus as claimed in any preceding claim,  
10      wherein the membrane is provided in the shape  
11      of a cylinder.  
12
- 13   15.    Apparatus as claimed in any preceding claim,  
14      wherein the membrane comprises one or more  
15      struts.  
16
- 17   16.    Apparatus as claimed in any preceding claim,  
18      wherein the support comprises alpha alumina.  
19
- 20   17.    A method of producing hydrogen gas, the method  
21      comprising:  
22        providing a membrane, the membrane comprising  
23        a support and a catalyst;  
24        passing a first reactant through the membrane  
25        from a first chamber to a second chamber;  
26        allowing the first reactant to come into  
27        contact with the catalyst upon passage through  
28        said membrane;  
29        imparting the first reactant with enough  
30        energy so as to react with the second  
31        reactant;

1       reacting the first reactant with a second  
2       reactant to produce hydrogen gas.

3

4     18. A method as claimed in claim 17, wherein the  
5       energy imparted on the first reactant  
6       activates molecules of the first reactant  
7       without forming an ionic species before the  
8       reaction with the second reactant.

9

10    19. A method as claimed in claim 17 or 18, wherein  
11       the temperature is over 500°C.

12

13    20. A method as claimed in claim 19, wherein the  
14       temperature is between 700°C and 800°C.

15

16    21. A method as claimed in any one of claims 17 to  
17       20, wherein the first reactant is one of  
18       oxygen and a hydrocarbon, and the second  
19       reactant is the other of oxygen and a  
20       hydrocarbon.

21

22    22. A method as claimed in claim 21, wherein the  
23       oxygen and hydrocarbon do not come into  
24       contact with each other until the first  
25       reactant has passed through said membrane from  
26       the first chamber to the second chamber.

27

28    23. A method as claimed in claim 21 or 22, wherein  
29       the hydrocarbon comprises a normally gaseous  
30       hydrocarbon.

31

1 24. A method as claimed in any one of claims 20 to  
2 wherein the pressure within the first  
3 chamber is greater than the pressure within  
4 the second chamber.

5

6 25. A method as claimed in any one of claims 20 to  
7 24, wherein carbon monoxide is formed in  
8 addition to the hydrogen.

9

10 26. A method as claimed in claim 25, wherein the  
11 carbon monoxide and hydrogen are further  
12 reacted to produce normally liquid  
13 hydrocarbons in a Fischer-Tropsch type  
14 reaction.

15

16 27. A method as claimed in any one of claims 20 to  
17 25, wherein the hydrogen is recovered for use  
18 as a fuel.

19

20 28. A method of preparing a membrane, the method  
21 comprising:  
22 providing a support; and  
23 adding a catalyst to the support.

24

25 29. A method as claimed in claim 28, wherein the  
26 support is an inorganic support.

27

28 30. A method as claimed in claim 28 or 29, further  
29 including the step of applying a coating to  
30 one of the surfaces of the support.

31

- 1    31.    A method as claimed in claim 30, wherein the  
2        coating produces a roughened surface on the  
3        support, said surface having an increased  
4        tortuosity compared to the tortuosity of the  
5        rest of the support.  
6
- 7    32.    A method as claimed in claim 30 or claim 31,  
8        wherein the coating comprises a metal oxide or  
9        metal oxide precursor.  
10
- 11   33.    A method as claimed in claim 32, wherein the  
12        metal oxide or precursor comprises a group IV  
13        metal oxide or group IV metal oxide precursor.  
14
- 15   34.    A method as claimed in claim 33, wherein the  
16        group IV metal oxide or precursor comprises  
17         $TiO_2$  or a  $TiO_2$  precursor.  
18
- 19   35.    A method as claimed in claim 30, wherein the  
20        coating produces a flux control layer on the  
21        membrane.  
22
- 23   36.    A method as claimed in any one of claims 30 to  
24        34, wherein a second coating, the second  
25        coating being a flux control layer, is also  
26        applied to the support.  
27
- 28   37.    A method as claimed in claim 35 or 36, wherein  
29        the flux control layer is applied to the  
30        membrane by exposure to a boemite sol.  
31

1    38.    A method as claimed in any one of claims 28 to  
2        36 wherein the coating and/or the second  
3        coating is applied by dipping the support into  
4        a liquid comprising the coating.

5

6    39.    A method as claimed in any one claims 28 to  
7        38, including the step of applying the  
8        catalyst to a surface of the membrane by  
9        passing a catalyst precursor solution over a  
10      first surface of the support and an osmotic  
11      solution over the opposite surface of the  
12      support, and allowing the catalyst or a  
13      catalyst precursor to be deposited on the  
14      support via the process of osmosis.

15

16    40.    A method as claimed in any one of claims 28 to  
17        39, further including the steps of drying the  
18      support and heating/firing the support.

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